# 國立交通大學 機械工程學系 碩士論文

FC-72 在水平矩形流道中流過一微小加熱面暫態流動 沸騰熱傳及氣泡特性研究

Transient Flow Boiling Heat Transfer of FC-72 and Associated Bubble Characteristics over a Small Heated Plate in a Horizontal Rectangular Channel

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中華民國九十六年六月

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國立交通大學

機械工程研究所 碩士論文初稿 A Thesis

Submitted to Institute of Mechanical Engineering

Collage of Engineering

National Chiao Tung University

In Partial Fulfillment of the Requirements

For the degree of

Master of Science

In

Mechanical Engineering

June 2007

Hsinchu, Taiwan, Republic of China

中華民國九十六年六月

# 國立交通大學

# 論文口試委員會審定書

本校\_機械工程\_學系碩士班\_楊政陞\_君

所提論文(中文) FC-72 在水平矩形流道中流過一微小加熱面暫態流動沸

騰熱傳及氣泡特性研究
(英文) Transient Flow Boiling Heat Transfer of FC-72 and Associated
Bubble Characteristics over a Small Heated Plate in a Horizontal
Rectangular Channel
合於碩士資格水準、業經本委員會評審認可。  「試委員: 何请这 「以及以上」 一番。
指導教授: 本人传授 教授

中華民國 96 年 6 月

8

日

幕然回首兩年前的此時,對於離家到新竹交大求學的我而言,心中真是充滿了既期待又害怕的複雜心情。來到交大這充滿學術研究氣息的生活,讓我覺得在此讀書做研究是一種享受。然而,一想到即將要離開這可愛的校園,不禁令人懷念起在此的點點滴滴。

能獲得碩士學位,首先很榮幸能接受林清發教授的指導,從文獻 資料的蒐集、實驗系統的構思設計到最後物理觀念的闡述分析,都令 我受益匪淺。而老師對我們在研究上嚴謹的要求,更深深地影響到我 日後的處事態度。而能夠順利地完成我的碩士論文,要感謝實驗室許 多臥虎藏龍的博士班:張文瑞、郭威伸、賴祐民、陳尚緯、謝汎鈞及 陳建安學長們的幫忙及指導。同學陳奎銘、李凱文、廖峻樟、黃宇歆 的互相砥礪幫忙,當然也少不了一群為實驗室注入活力、帶來歡樂的 學弟妹們:林永龍、王壹龍、李浚圩及駱長志的幫忙。得之於人者太 多,在此一同向所有幫助過我的人致謝。

即將踏出交大校門成為社會新鮮人的我,回首來時路,很慶幸並沒辜負當初父母對我的期望;在今年能如期獲得碩士學位。我想今天若我有任何些微的成就,父母對我的教養及支持鼓勵,是我能一路走來的原動力,僅將我的榮耀獻予我摯愛的家人。

楊政陞 2007/6 於風城交大

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#### 摘要

本實驗是要探討雙相流冷媒循環系統針對介電冷卻液 FC-72 在截面爲寬 20 毫米、高 5 毫米之水平矩形流道(水力直徑爲 8 毫米)中進行,隨時間週期振盪的流量如何影響暫態強制對流沸騰熱傳以及相關的氣泡特徵,加熱銅塊埋至於測試段之底板中央其尺寸爲直徑 10 毫米。值得注意的是冷卻液流量隨時間振盪(振盪的形狀接近三角波),是如何影響暫態流動沸騰將會被詳細的探討。在實驗參數範圍上,介電液 FC-72 平均質量通率從 300 到 400 kg/m²s 而且流量的振盪振幅爲 0%、5%、10%,流量的振盪周期爲 10 秒到 30 秒。除此之外,FC-72 於測試段入口處次冷度從 0 到 10 °C、銅塊的加熱通量從 0.1 到 10 W/cm² 而系統壓力爲常壓。

由實驗結果發現介電冷卻液的振盪振幅和週期對時間平均的 FC-72 暫態的飽和態和次冷態流動沸騰熱傳特徵沒有明顯的影響,類似穩態的流動沸騰。無論如何,在熱通量高於起始成核沸騰的熱通量 FC-72 的暫態飽和態和次冷態流動沸騰對熱傳係數、氣泡脫離直徑、氣泡脫離頻率、成核址密度都有顯著的振盪影響。除此之外,在高熱通量下和振盪振幅比較大的情況下對熱傳係數、氣泡脫離直徑、氣泡脫離頻率、成核址密度都會造成更強烈的振盪情況發生,但振盪週期的影響並不明顯。因此,當流量隨時間增加的情況下,氣泡脫離的尺寸和成核址密度都會下降,但氣泡脫離頻率會增加。當流量隨時間遞減的情況下,會產生相反的趨勢。並且也發現入口處次冷度的增加會使得沸騰的熱傳係數振盪更劇烈。

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Transient Flow Boiling Heat Transfer of FC-72 and Associated

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**Rectangular Channel** 

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**Institute of Mechanical Engineering** 

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**ABSTRACT** 

This study intends to explore how a time periodic coolant flow rate affects the

transient forced convective boiling heat transfer and associated bubble characteristics

of FC-72 over a small heated circular copper plate flush mounted on the bottom of a

horizontal rectangular channel with a cross section of 20 mm in width and 5 mm in

height. The diameter of the copper plate is 10 mm. More specifically, the effects of

the coolant flow rate oscillation in the form of nearly triangular wave on the transient

flow boiling will be examined in detail. In the experiment the time-average coolant

mass flux  $\overline{G}$  is varied from 300 to 400 kg/m<sup>2</sup>s and the amplitude of the coolant mass

flux oscillation is fixed at 0%, 5% and 10% of  $\overline{G}$ . The period of the coolant mass

flux oscillation varies from 10s to 30s. Besides, the liquid subcooling at the inlet of

the channel ranges from 0°C to 10°C and the heat flux imposed on the heated plate

varies from 0.1 to 10 W/cm<sup>2</sup>.

The experimental results show that the time-average data of the FC-72 transient

saturated and subcooled flow boiling heat transfer characteristics are not affected to a

significant degree by the amplitude and period of the coolant mass flux oscillation. In

fact, they resemble these for the stable flow boiling. However, in the transient

saturated and subccoled flow boiling of FC-72 significant temporal oscillations in the boiling heat transfer coefficient, bubble departure diameter and frequency, and active nucleation site density appear for the imposed heat flux slightly higher than that for ONB. They oscillate at the same frequency as the mass flux oscillation. Besides, at a higher imposed heat flux and for a larger amplitude of the mass flux oscillation stronger oscillations in  $h_{2\phi}$ ,  $d_p$ , f and  $N_{ac}$  are noted. But they are only slightly affected by the period of the mass flux oscillation. Furthermore, in the time duration in which the mass flux rises with time both the size of the departing bubbles and active nucleation site density decrease, but the bubble departure frequency increases. The opposite processes occur for a sink of mass flux with time. We also note that an increases in the inlet liquid subcooling causes stronger oscillations in the boiling heat transfer coefficient.

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## **NOMENCLATURE**

A area, m<sup>2</sup>

B element height, m

 $c_p$  specific heat,  $J/kg^{\circ}C$ 

D hydraulic diameter of rectangular-channel, m

G mass flux, kg/m<sup>2</sup>s

g acceleration due to gravity, m/s<sup>2</sup>

H height, m

h heat transfer coefficient,  $W/m^2 \cdot K$ 

I measured current from DC power supply, A

i<sub>lv</sub> enthalpy of vaporization, J/kg·K

k thermal conductivity, W/m·K

L length, mm

 $\dot{m}$  mass flow rate, kg/s

 $\mbox{Ja'} \qquad \mbox{Jacob number based on } \Delta T_{sub}, \ \mbox{Ja'} = \frac{\rho_l \cdot C_{pl} \cdot \Delta T_{sub}}{\rho_v \cdot i_{lv}} \, , \, \mbox{dimensionless}$ 

Nu Nusselt number,  $Nu = \frac{h \cdot L}{k}$ , dimensionless

P system pressure, kPa

Pr Prandtl number,  $Pr = \frac{\mu \cdot C_p}{k}$ , dimensionless

N<sub>ac</sub> Active nucleation site density, n/m<sup>2</sup>

Q heat transfer rate, W

q average imposed heat flux, W/cm<sup>2</sup>

Re Reynolds number,  $Re = \frac{G \cdot D}{\mu}$ , dimensionless

S element space between two adjacent elements, m

T temperature, °C

V coolant FC-72 flow velocity, m/s

V measured voltage from DC power supply, V

W width, m

## **Greek Symbols**

 $\Delta T$  temperature difference,

 $\mu$  dynamic viscosity,  $N \cdot s/m^2$ 

v specific volume, m<sup>3</sup>/kg

ρ density, kg/m<sup>3</sup>

ε relative heat loss, dimensionless

## Subscripts

ave average

c,h from heater surface to cooper surface

cop copper

cs cross-section of rectangular-channel

d diameter

xxxii

e effective

f fin

fin mean bubble departure frequency

g gas

h hydraulic

i at the inlet of the test section

in at the inlet of the test section

i,o at inlet and exit of the test section

1 all-liquid nonboiling heat transfer

lv liquid phase to vapor phase

m average value for the two phase mixture or between the inlet and exit

M mica

n

net power input to the coolant FC-72

n active nucleation site density

o at the outlet of the test section

p preheater

pool pool boiling

r coolant FC-72

s surface

sat saturated state for coolant FC-72

sp single-phase convective heat transfer

sub subcooled state for coolant FC-72

T teflon

t total

t-g thermal-grease

tp two-phase boiling heat transfer

v vapor

w wall

w water

1φ single-phase

2φ two-phase

